

Figure 1

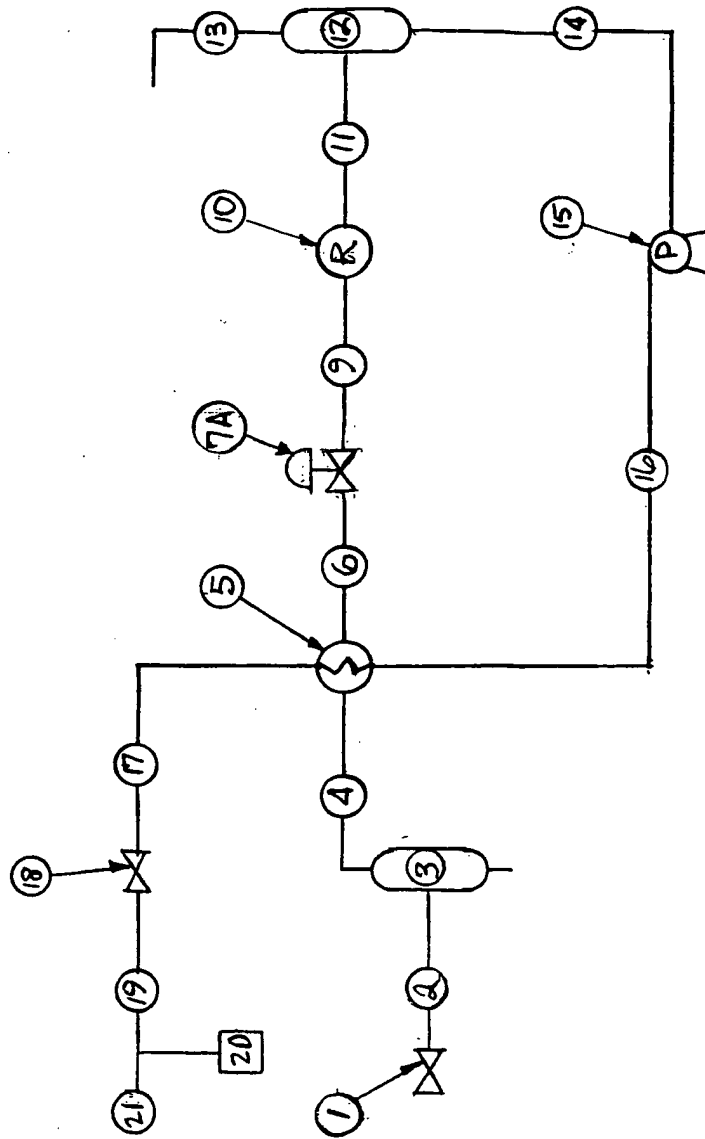
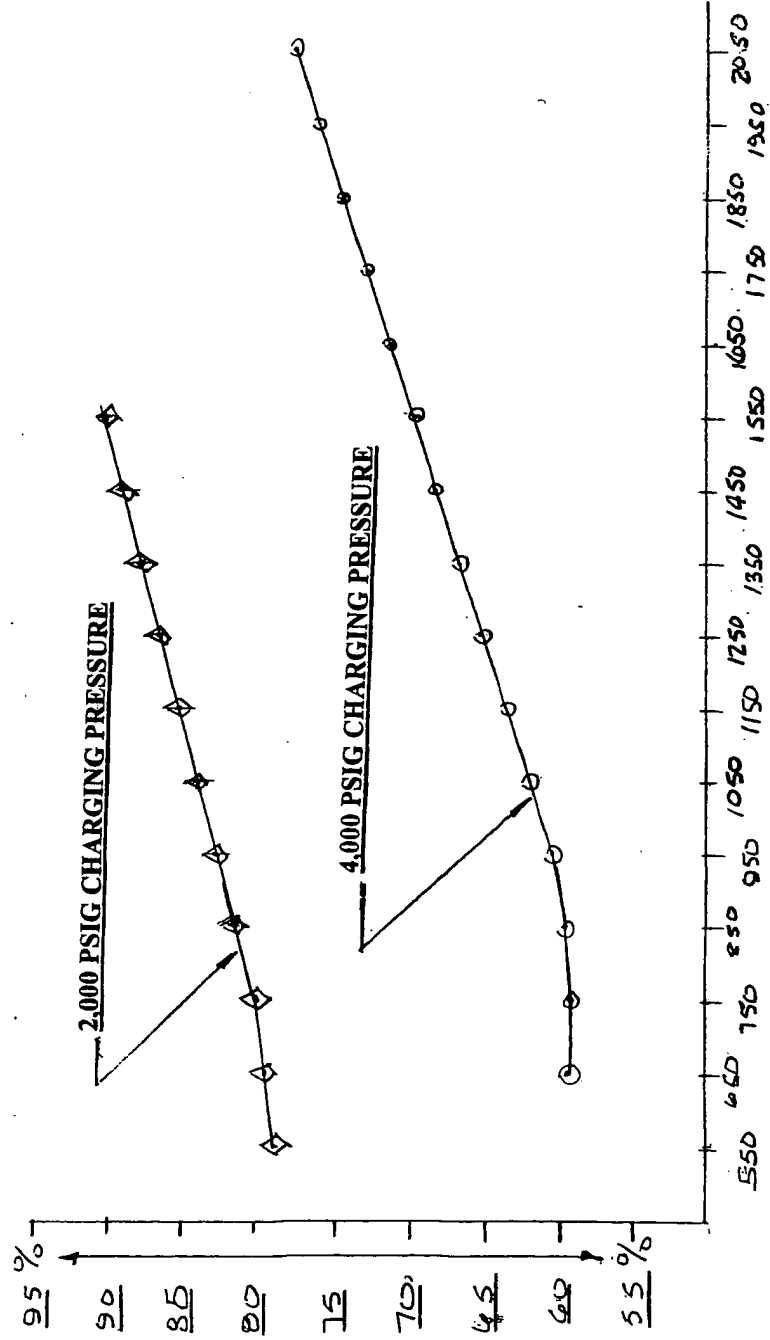


Figure 2

REFRIGERATION ENERGY RECOVERY
PERCENT OF TOTAL REQUIRED LIQUEFACTION ENERGY



INLET NATURAL GAS STREAM PRESSURE TO IC-LNG PROCESS STREAM

Figure 3

Illustrates, the Refrigeration energy recovery by the IC-LNG Process System, as a percent of the total liquefaction energy required versus various inlet natural gas pressures to the IC-LNG Process System, for developing charging pressures of 2,000 psig and 4,000 psig, when using the Turbo-Expander Device. Illustration figure is based on a natural gas flow rate to IC-LNG Process System of 80 mmscfd.

Figure 4

Illustrates, the difference in Horse Power required for a Gas Compressor System versus the IC-LNG Process System, using a Turbo-Expander Isentropic Expansion device to charge (pressurize) natural gas storage reservoir facilities and or storage containers to 2,000 psig. Illustration figure is based on a natural gas flow rate to the IC-LNG Process System of 80 mmscfd.

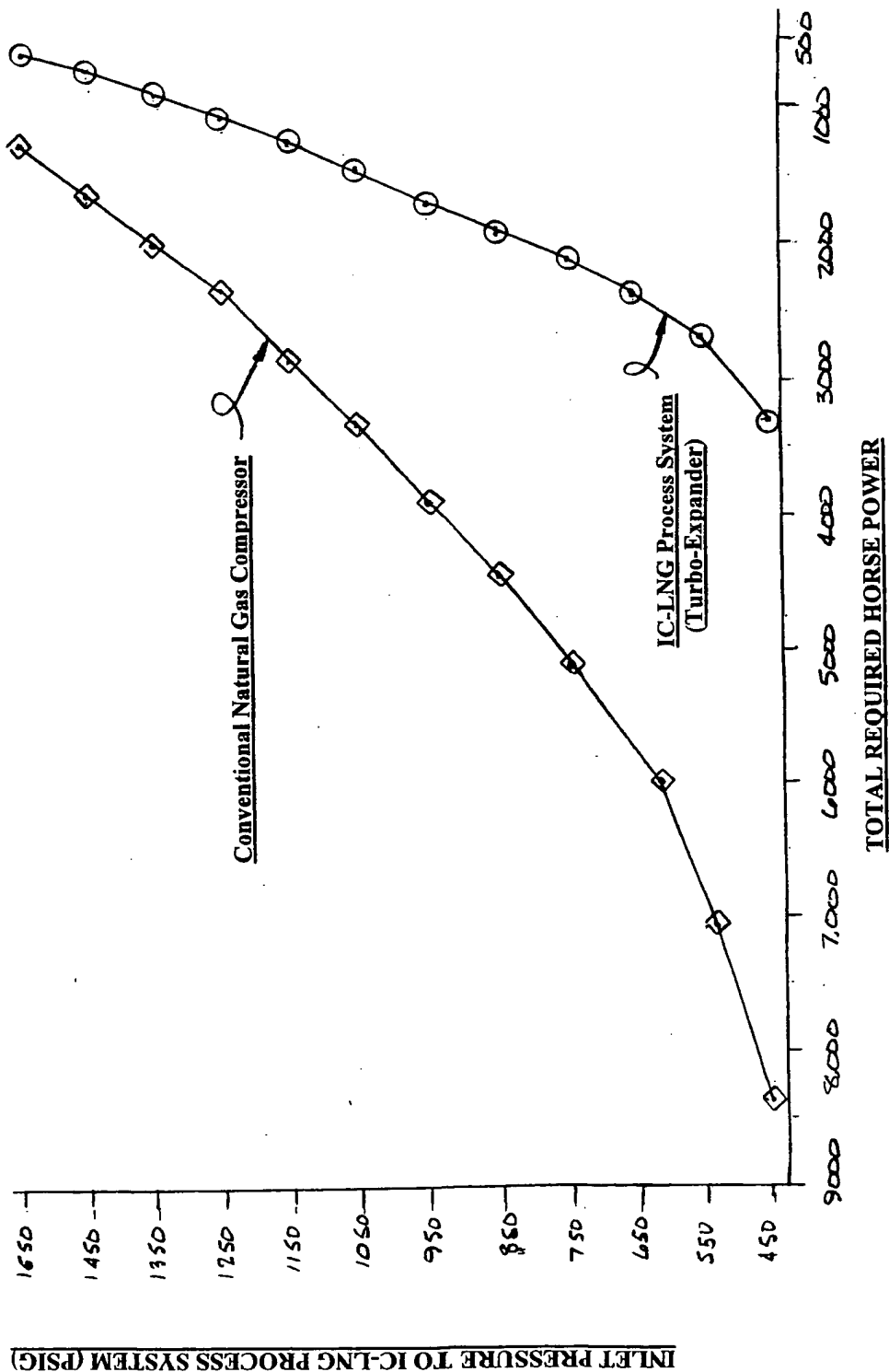


Figure 5

Illustrates, the difference in Horse Power required between a Gas Compressor System and the IC-LNG Process System, using a Joule-Thomson" Isenthalpic expansion valve to charge (pressurize) natural gas storage reservoir facilities and or storage container systems to 2,000 psig. Illustration figure is based on a natural gas flow rate to the IC-LNG Process System of 80 mmscfd.

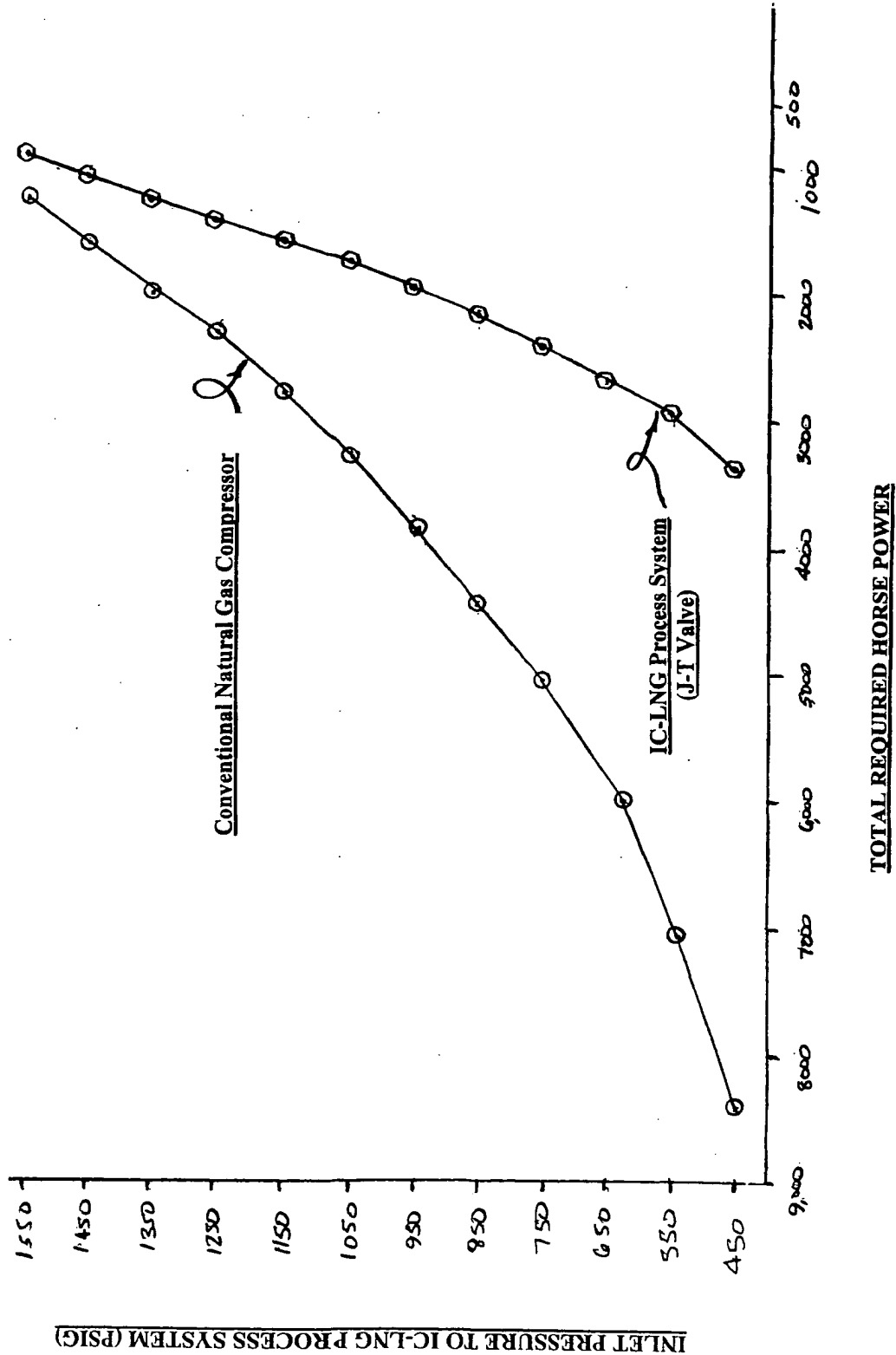


Figure 6

Illustrates, the difference in Horse Power requirements between a Gas Compressor System and the IC-LNG Turbo-Expander Process System to charge (pressurize) natural gas reservoir facilities and or storage container systems to 4,000 psig. Illustration figure is based on a natural gas flow rate to the IC-LNG Process System of 80 mmscfd.

